



Bioscience, Inc.

Environmental Products & Services ISO 9001:2008

# Hydrogen Sulfide (H<sub>2</sub>S) Control Cost Savings in a Municipal Sewer Collection System and Treatment Plant

*Odor and Corrosion Control in Pump Stations Using Microcat<sup>®</sup> - ANL BioBlend - BSE 124*



## Multi-Year Evaluation Program

Evaluation of sewer bioaugmentation with MICROCAT – ANL BioBlend for hydrogen sulfide (H<sub>2</sub>S) control in this sewer system was undertaken in two cycles over a two year period. Year One results were excellent, and additional Year Two full-scale product applications confirmed both the Year One results and the cost savings for switching from nitrate chemical addition methods to natural, biological methods of H<sub>2</sub>S control. In Year Three, the switch was made to MICROCAT – ANL BioBlend despite physical changes in the sewer system and mechanical difficulties with the H<sub>2</sub>S monitoring system.

## Problem - Year One

Hydrogen sulfide generated in sewer systems can cause safety and maintenance problems including toxicity to humans, odors and corrosion. Several methods are used to control H<sub>2</sub>S in collection systems. While many have proven to be at least partially effective, they can be quite costly and require constant attention in order to exert sufficient control to keep the costs to a minimum without sacrificing performance.

In these lift stations the H<sub>2</sub>S levels were such that under certain conditions the installed nitrate chemical control technique could not keep up with the chemical demanded and hazardous H<sub>2</sub>S levels in the lift station atmosphere could not be avoided from time to time. Nitrate dosing could be increased, but the response was slow and the costs were deemed to be excessive. Therefore, a better, less expensive and more environmentally sound control method was sought.

The objective of this program was to determine the effectiveness of applying MICROCAT-ANL microbial sulfide controller for keeping the H<sub>2</sub>S levels below 10 ppm in the air at a full-scale pump station. If the application proved effective, then a further objective was to determine how much could be saved using the MICROCAT product in comparison to the nitrate chemical product then in use.

## Application Procedure

---

Based on the sewer system layout, length of sewer lines from Pump Station 1 and Pump Station 2 to Pump Station 3, daily average flow rate and hydraulic retention times, an application methodology was developed to inoculate Pump Stations 1 & 2, leading to Pump Station 3 where H<sub>2</sub>S measurements would be taken.

### Pump Station 1:

Start-up dosing during 5 days:	0.05 Gallons/day	(0.177 L/day)
Maintenance dosing following the start-up period:	0.02 Gallons/day	(0.089 L/day)

### Pump Station 2:

Start-up dosing during 5 days:	1 Gallon/day	(3.79 L/day)
Maintenance dosing following the start-up period:	0.5 Gallons/day	(1.89 L/day)

Product application two times per day was started on the 16<sup>th</sup> of April using programmable peristaltic pumps. The only required additional equipment at both application points was a 5 gallon (approximately 20 L) product container. MICROCAT-ANL is stable and non-hazardous, so no special storage conditions or safety precautions are needed.

On the 15<sup>th</sup> of May MICROCAT – ANL application was switched off to see if the treatment had a prolonged effect after product application stopped. On the 22<sup>nd</sup> of May it was switched on again.

## Results and Conclusions

---

The first graph below displays H<sub>2</sub>S levels measured at Pump Station 3 from the 1<sup>st</sup> of April to the 31<sup>st</sup> of October. The graph displays the hourly average H<sub>2</sub>S concentration. The second graph shows the H<sub>2</sub>S development at Pump Station 3 during the period of interrupted application of MICROCAT - ANL. H<sub>2</sub>S levels stay below the 10 ppm limit during most of the evaluation period. During the period of interruption from May 15<sup>th</sup> to May 22<sup>nd</sup>, H<sub>2</sub>S levels increased slowly until the 5<sup>th</sup> of June when the ANL treatment was fully reactivated, and H<sub>2</sub>S levels started to come down again.

From the middle of July significantly warmer weather began and lasted up to the middle of September. This pushed H<sub>2</sub>S levels up. However, for most of this period H<sub>2</sub>S levels in Station 3 stayed below 10 ppm. On several instances H<sub>2</sub>S levels rose over 10 ppm but stayed close to the 10 ppm target and reverted to the target quickly without increasing the dosing of the MICROCAT - ANL product.

The second graph focuses on the period during which the application of MICROCAT – ANL was purposely turned off (May 15 to May 22) and the response when it was restarted on May 23.

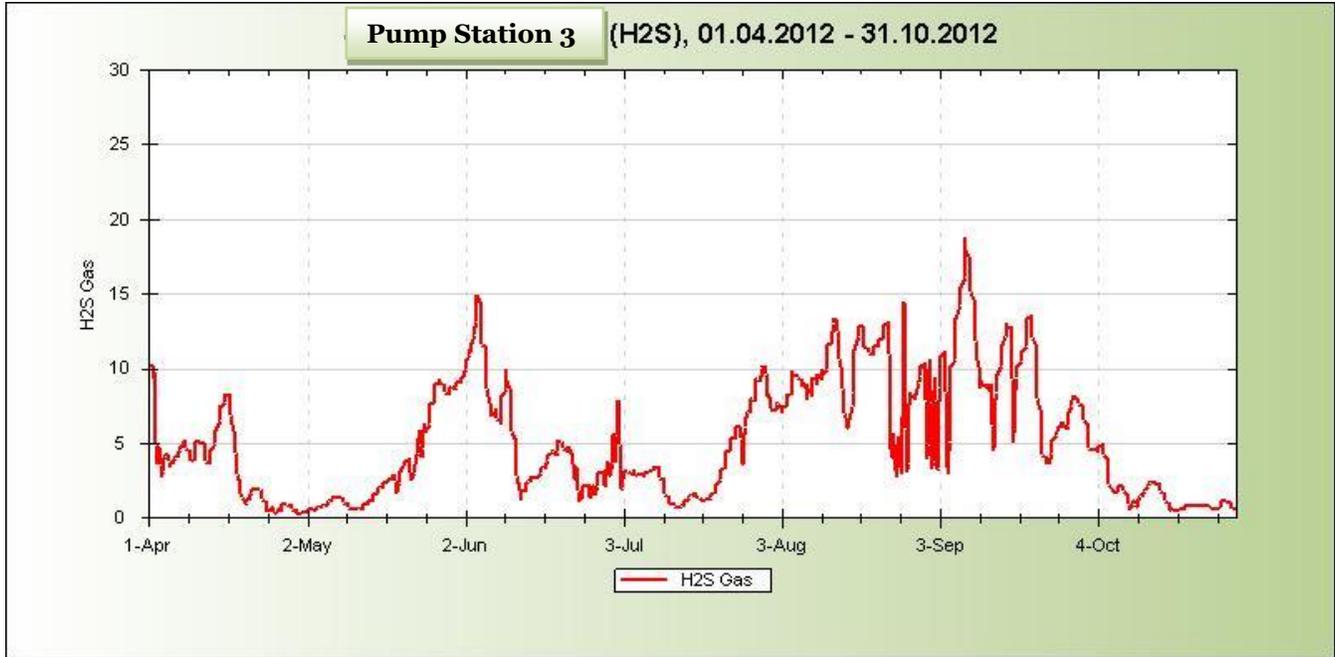
The Microcat-ANL application program demonstrated that biological H<sub>2</sub>S control is a viable method of controlling the emission of sewage gas and can keep H<sub>2</sub>S levels within acceptable safety and corrosion limits.

As the application volume of the liquid ANL product is a constant set amount and not controlled by H<sub>2</sub>S loggers, the annual product consumption can be easily calculated beforehand. This eliminates the possibility of exceeding the allocated budget for the H<sub>2</sub>S control. MICROCAT -ANL is non-hazardous, so storage conditions can be relatively simple and it poses no risk to workers on site.

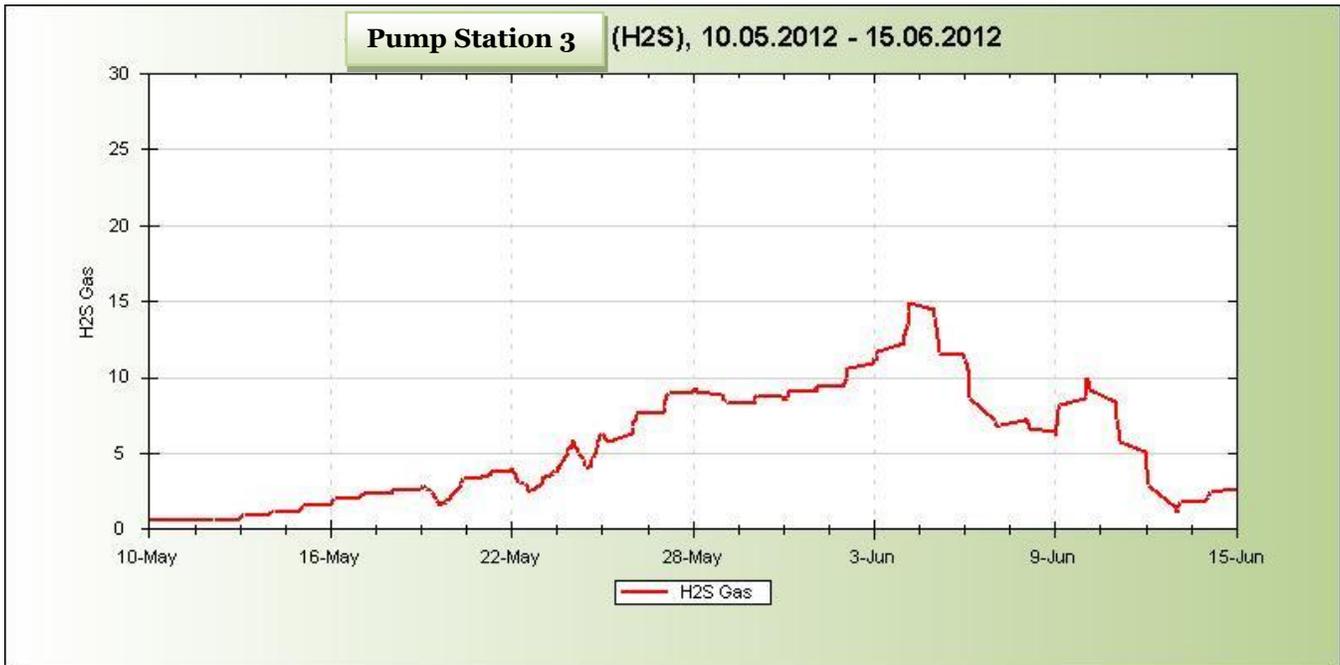
Total MICROCAT-ANL consumption during the evaluation period was 100 gallons (382 L) including the 5 day start-up. Due to the interruption of product application in May an additional 5 gallons (19.8 L) was used to restart the application program. A full year of MICROCAT-ANL treatment will consume 182 gallons (722 L), not including start-up usage. Thus, an annual MICROCAT-ANL cost was calculated to be about 50% less than the nitrate chemical program in use.

---

## Additional Benefits



Based on applications of MICROCAT-ANL at other locations there are additional benefits at the downstream wastewater treatment plant when the product is used in the upstream collection system. Reduced oxygen demand (BOD), improved solids settling (lower sludge volume index), reduced odor from primary clarifiers and the headworks in general, and from sludge dewatering operations have been documented. These improvements in performance can lead to additional operating cost savings.



## Problem - Year Two

---

The objective of this follow-on program was similar to that in Year One, namely to determine whether H<sub>2</sub>S control to a 10 ppm standard using MICROCAT – ANL could be achieved at a downstream wastewater treatment plant (WWTP), and, if so, how much could be saved by switching from nitrate chemical sulfide control to natural, biological sulfide control. In this case H<sub>2</sub>S levels were monitored at the inlet headworks to the municipal wastewater treatment plan (with a population equivalent of about 14,600) where H<sub>2</sub>S in the air often exceeded the target level of 10 ppm or less. Two upstream pumping stations discharging into the WWTP were treated:

**Pump Station 1 – Operating Volume 1320 gallons (5 m<sup>3</sup>)**

Flow rate: 0.4 gallons/second (1.5 liters/second)

**Pump Station 2 – Operating Volume 9240 gallons (35 m<sup>3</sup>)**

Flow rate: 52.8 gallons/second (200 liters/second)

## Application Program

---

The application program ran from March 25 to May 27. H<sub>2</sub>S levels were monitored using 3 different monitors at 3 different points near the sewer line discharge into the headworks of the WWTP.

## Results

---

The overall results are shown in Table 1. Note that Monitors A and C had previously exhibited inconsistent operation and errors in measurement. Therefore, the customer decided to use the data from Monitor B for determining the results of this evaluation.

**Table 1 – Summary of H<sub>2</sub>S levels (after stabilizing period) from March 25<sup>th</sup> to May 27<sup>th</sup>**

H <sub>2</sub> S levels	Monitor A	Monitor B	Monitor C
<b>Average</b>	0.74 ppm	1.75 ppm	2.86 ppm
<b>Min</b>	0 ppm	0 ppm	0 ppm
<b>Max</b>	18 ppm	30 ppm	31.1 ppm
<b>95 percentile</b>	4 ppm	4.4 ppm	12.8 ppm

The customer concluded that the evaluation proved that “MICROCAT - ANL Bio Blend can achieve the target H<sub>2</sub>S level of 10 ppm or less 95% of the time based on the data from Monitor B”.

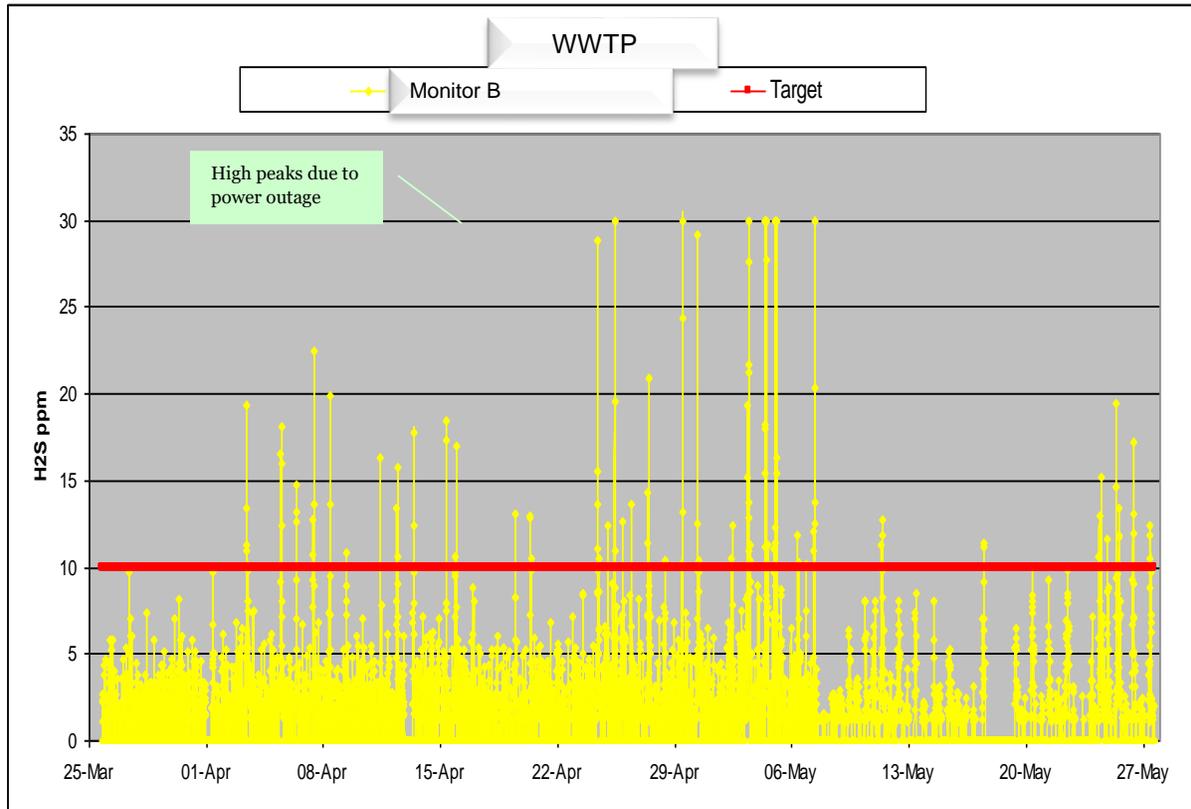


Figure 1: H<sub>2</sub>S levels at WWTP inlet screens for full evaluation period

## Cost Savings

The application rate of MICROCAT - ANL BioBlend needed for effective, on-going bioaugmentation treatment of Pump Stations 1 and 2 was determined to be 1.3 gallons per day (5 liters per day) April through October and 0.8 gallons per day (3 liters per day) November through March for each pump station. This equated to a savings of about \$2000 per annum in product cost compared to chemical dosing excluding delivery and service/maintenance costs. This was a bit misleading since the MICROCAT – ANL product price included delivery, maintenance and dosing equipment, so the overall savings was much higher. In addition to chemical costs, the customer was paying approximately \$9,000.00 per annum in service fees plus a chemical delivery charge of \$17,000 per annum. Thus, per Table 2 the actual overall savings rose to \$28,000.00 per year or about 41% less per year than the total cost of chemical addition (Table 2).

Table 2 –Nitrates vs. MICROCAT - ANL Cost Comparison

	Nitrates	MICROCAT - ANL	ANL Savings
<b>Yearly application cost, total</b>	<b>\$42,234.00</b>	<b>\$40,186.00</b>	
Application cost saving per year		\$2,048.00	5%
<b>Yearly service fee</b>	\$9,000.00	n/a	
<b>Product delivery charges</b>	\$16,965.00	n/a	
<b>Total cost per year</b>	<b>\$68,199.00</b>	<b>\$40,186.50</b>	<b>41%</b>

Work continues at the site to determine potential additional benefits of sewer line bioaugmentation for H<sub>2</sub>S control in the WWTP. To date both improved and reduced WWTP performance have been observed, but neither can be definitively correlated with the sewer bioaugmentation.

## Implementation - Year Three

---

The final section of sewer line (gravity sewer) was replaced from where the 2 force main sewers coming from the two main pumping stations joined and which ended at the central treatment plant. The new line is a 600 mm and Poly pipes PVC whereas the old line was a concrete pipe. The line was replaced without notifying the product supplier nor those responsible for the H<sub>2</sub>S control.

During the replacement the sewage was diverted towards the treatment plant via a temporary line. During and after the installation of the new pipe H<sub>2</sub>S levels in the inlet screening building started to rise. Also, the turbidity of the final effluent of the treatment plant increased and more aeration power was required. This indicated the rise of sulfide concentration in the influent.

Due to the removal of the old sewer line the already established ANL biofilm was removed and the product supplier initiated a new start up program (double dose) in order to reestablish the biofilm in the new section. Although the turbidity of the final effluent of the treatment plant quickly improved and aeration power was reduced again, there was no effect on the H<sub>2</sub>S in the screening building. Target H<sub>2</sub>S levels in this building should remain below 10 ppm for 95% of the time. At times H<sub>2</sub>S levels spiked well over 30 ppm. As the months passed there was no improvement in H<sub>2</sub>S levels and triple dosing was implemented. A meeting was called to discuss the progress toward achieving hydrogen sulfide treatment goals.

Simultaneously, the company responsible for maintaining the air filters in the screening building performed maintenance on the filters and noticed that the ventilation of the building was very poor due to blockages in the filter system. As soon as these blockages were removed, the H<sub>2</sub>S levels in the screening building dropped significantly and were below the 10 ppm again in accord with prior results.

It was concluded that the increase of H<sub>2</sub>S was not due to MICROCAT-ANL performance but due to the fact the filter system of the screening building was blocked and allowed H<sub>2</sub>S levels to build up due to improper ventilation. As soon as the ventilation system was repaired and the blockages removed the H<sub>2</sub>S levels dropped to the levels achieved before of the sewer line replacement.

The main treatment plant operator also reported:

*“Just thought I would let you all know that the site is over the worst of problems. The odor plant is now extracting and H<sub>2</sub>S is much improved. The dissolved oxygen (DO) is reaching set points so blowers are more relaxed. Final (effluent) is very good, mixed liquor is back to normal and thickening well.”*